Electrospun Polyurethane/ß-Cyclodextrin Composite Membranes for Aerosol Filtration and Adsorption of Volatile Organic Compounds from the Air

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A R T I C L E   I N F O

ORIGINAL ARTICLE

ABSTRACT

Introduction: Electrospun nanomembranes have been used for effective air filtration due to their potential for active surface modification. This study aims to synthesize polyurethane (PU) nanofiber membrane incorporated with different amounts of β-cyclodextrin (β-CD) to capture volatile organic compounds (VOCs) along with aerosol filtration from the air.

Material and Methods: First, PU was synthesized by MDI method. A 10 wt% PU solution in DMF/MEK (1:1 wt) was prepared. Various amounts of β-CD powder (0, 1, 2, 3, and 5 wt% of PU) were dispersed in the prepared PU solution. Electrospining process was carried out under determined parameters (20 kV applied voltage, tip-to-collector distance of 10 cm, solution feed, and rate of 1 ml/h). The chemical structure and morphology of the produced samples were assessed by FTIR and SEM, respectively. Finally, air filtration and toluene adsorption of different electrospun membranes were measured.

Results: The highest filtration performance was observed for PU with 1 wt% β-CD nanofiber. Due to increased efficiency (83.13%) and low-pressure drop (ΔP = 19 pa), this sample had a considerable quality parameter. The results demonstrated that the membrane loaded with β-CD was able to adsorb hazardous and carcinogenic VOCs. It was confirmed that adding β-CD into PU improves the adsorption capacity due to forming a π complex and having a different tendency against capturing a variety of VOCs.

Conclusion: The study results revealed that the PU nanofiber incorporated with β-CD, along with the ease of regeneration, can make them attractive for air filtration and VOCs adsorption.

Introduction

Air pollution is a global issue threatening human lives and the environment[1,2]. Classification of air pollutants which ranges from suspended particles to gaseous versus particulate pollutants, recognizing and applying appropriate methods and equipment to decrease or eliminate contaminants. Particulate matter (PM) refers to solid and liquid particles suspended in the air with various sizes and compositions emitted from different sources[3]. Man-made activities, such as industrial processes, vehicle emissions, and even indoor activities can cause the emission of aerosol and volatile organic compounds (VOCs). PM are classified into 3 groups, including $PM_{0.1}$ (smaller than 0.1 μm), $PM_{2.5}$ (0.1 – 2.5 μm), and PM_{10} (2.5-10 μm)[4]. Fine particles, owing to their small size, are more respirable and can penetrate the lower respiratory

system. If the particles are small enough, they can penetrate pulmonary alveoli and then be transmitted into the circulatory system, resulting in serious consequences. Epidemiological studies demonstrate significant relation between cardiorespiratory morbidity and mortality with exposure of $PM_{2.5}$ and PM_{10}[5-7].

VOCs are an expanded spectrum of organic compounds with a boiling point of 50-260 ℃ at atmospheric pressure. Due to lower boiling temperatures, evaporations rapidly spread out in indoor and outdoor space. Therefore, they have been considered as the most important air contaminant[8]. People working in areas in contact with VOCs, are significantly exposed to the compounds through inhalation[9]. The adverse effects of VOCs cause skin irritation, respiratory problems, and cancer (in case of long-term exposure)[10]. Purification of breathing air at indoor exposures is one of the important issues. Filtration is one of the most considerable mechanisms of purifying the air from different types of contaminants[11]. Many air filtration materials have been developed, such as glass fiber[12], activated carbon (AC) fiber[13] (which is considered to be one of the best air purification materials due to its unique features), nanometer fiber[14], and film compound filter materials[15]. Non-woven fibers have been identified as efficient absorbents in nanometer-scale due to the smaller diameters, high surface area and porosity, low weight, and good internal connectivity[16-18]. Electrospinning is a simple and cost-effective approach that leads to the fabrication of non-woven nanofiber membranes. It is also known as an efficient approach for synthesizing fiber membranes with high-performance air filter application[19,20]. A set of common polymers commercially have been used in the electrospinning process, such as PAN[21,22], Poly (L-lactic) acid[23], polyurethane (PU)[24], and cellulose acetate[25]. Among these, electrospun PU membranes have been extensively known for their good elasticity and mechanical strength[26].

Since pure polymeric electrospun nanofibers without modification have very low adsorption capacities of gases, an additional step of treatment is required for their acceptable performance. In most cases, the incorporation of nanoparticles into a polymeric solution results in constrictive modifications in nanofiber's morphology and diameter characteristics, which leads to the generation of high-efficiency filter membranes. Kim et al. demonstrated that the PU electrospun nanofiber mat incorporated with fly ash nanoparticles has a significant adsorption capacity against VOCs compared to pure PU nanofiber mat[27]. Cyclodextrins are a family of cyclic oligosaccharides with a hydrophobic interior and hydrophilic exterior, in which the glucopyranose units are joined by α-1, 4 bonds. Among different types of cyclodextrin, β-cyclodextrin (β-CD) (as a commercially biological supermolecule[28]) has the advantages of being non-toxic, cost-effective, and most available compared to other cyclodextrins[29,30]. In its chemical structure, seven glucose units have surrounded the hydrophobic cavity[31-33]. One of the noticeable characteristics of β-CD is the formation of complex properties with many other components[34,35]. β-CD (host) cavities provide a connection ring shape location for non-polar and suitable guest molecules, which end up in complex formation[36]. The most appropriate guest components which are accepted by β-CD as host include alcohols, aldehydes, ketones, fatty acids, other organic acids, gases, and also VOCs, such as styrene, aniline, and toluene as well as formaldehyde[37]. Among expanded applications of this electrospun membrane, filtration of breathing air against any fine particles and toxic gases and vapors is another unique application of these membranes. Cartridges of common protective respiratory masks are packed with AC granolas, which adsorb contaminants. Despite nanofiber high surface area and excellent adsorption, the considerable weight of the cartridge part due to presence of AC, applies excessive load and stress to neck muscles, leading to uncomforted condition for user. Therefore, replacement of conventional filter cartridges by low-weight electrospun nanofibers with adequate efficiency can be a good solution.

Herein, PU was synthesized based on PTMG and MDI. Then, β-CD-incorporated PU composite nanofibers were fabricated using electrospinning process. The physico-chemical characteristics of nanofibers were analyzed by appropriate tools. Finally, simultaneous air filtration and VOC adsorption of the pure PU and β-CD/PU nanofibers were measured.

Materials and Methods

Polytetramethylene ether glycol (PTMG) with M_w = 2000gr/mol, 1, 4-butanediol (BD), and 4, 4- Methylene diphenyl diisocyanate (MDI) was purchased from Sigma Aldrich (USA). The utilized liquids were dibutyltin dilaurate, B-cyclodextrin, dimethylformamide, dry toluene, dibutylamine, isopropyl alcohol, bromophenol blue, ethyl methyl ketone, HCl 0.01 N, and dried tetrahydrofuran, all supplied by Merck Co. (Germany).

Preparation of PU samples

First of all, dehumidification of PTMG and 1, 4-butanediol was carried out through a vacuum oven at 70 ℃ for 3 h and 40 ℃ for 1h, respectively. DMF was distilled under the 200 mbar vacuum at 105 ℃. A certain amount of distilled MDI (69.2 mmol) was mixed with 200 ml of dried tetrahydrofuran solvent, and under the dry nitrogen flow, it was purged into a certain amount of PTMG alcohol (13.8 mmol) and 0.1 ml of dibutyltin dilaurate. Then, the mixture was heated (Figure 1 (a)) [38].

Calculation of reaction progress

The reaction progress evaluation was carried out by ASTM D2572 standard test method. 1.1 mEq of NCO was transferred into 250 cc Erlenmeyer and 25 cc toluene was added. The mixture was stirred for 20 min while it was covered by a lid. 25 cc of dibutyl amine 0.1 N was added into the mixture and again stirred for 15 min with a closed lid.

Then, 100 cc of isopropyl alcohol and 4-6 drops of bromophenol blue marker were introduced. Finally, it was tittered by HCL 0.01 N. These steps were carried out for a blank sample. The reaction was carried out until the theoretical isocyanate content determined by di-n-butyl amine titration was reached. % NCO was calculated by Equation 1 [38].

$$\% \text{ NCO} = \frac{[(B-V) \times N \times 0.042]}{W} \times 100 \tag{1}$$

In which, B and V indicates the volume of HCL for titration of blank (cc) and volume of HCL for titration of the sample (cc), respectively. Also, N and W show the normality of HCL and grams of the sample weight (gr). The constant number 0.042 refers to the miliequivalent weight of the NCO group.

Solution preparation

A 10 wt% PU solution in DMF/MEK (1:1 wt) was prepared using a magnetic stirrer with 300 rpm for 12 h at ambient temperature (Figure 1(b)). Various amounts of β-CD powder (0, 1, 2, 3, and 5 wt% of PU) were dispersed by ultrasonication for 15 min to attain a homogenous solution (Figure 1(c)).

Electrospinning

The electrospinning setup (Figure 2) was comprised of three main parts, including a high voltage power supply, a syringe pump, and a ground electrode collector. The employed electrospinning parameters were 20 kV applied voltage, tip-to-collector distance of 10 cm, solution feed rate of 1 ml/h, and collector rotation rate of 300 rpm. Nanofibers with varied densities were prepared by changing the electrospinning duration. After electrospinning, all membranes were dried in a vacuum oven for 4 h at 50 ℃.
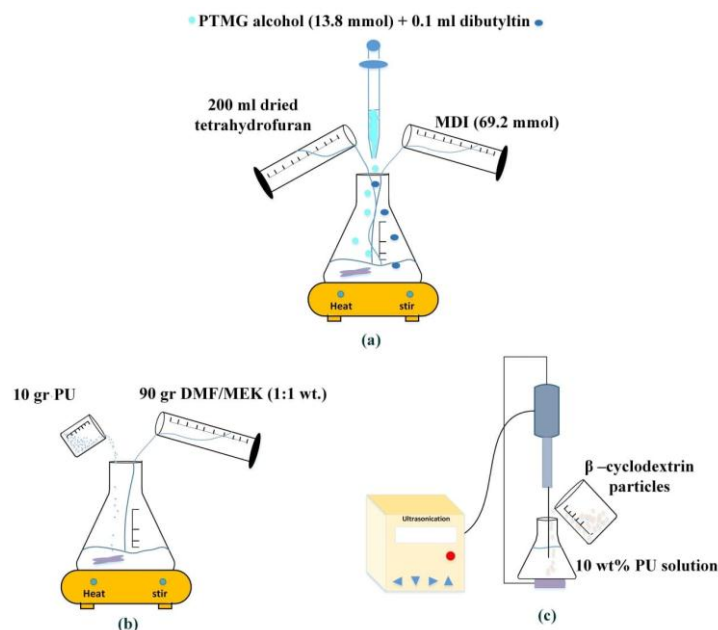
Figure 1: (a) Preparation of PU sample, (b) PU solution preparation, and (c) PU/β-cyclodextrin solution preparation
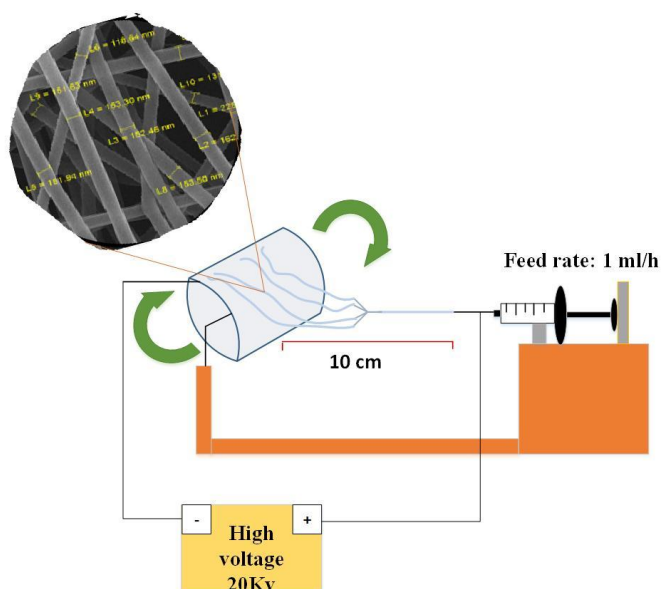

Figure 2: Electrospinning of nanofiber membrane

Characterization of electrospun nanofibers

The Fourier-transform infrared spectroscopy (FTIR) spectra of samples were recorded using an Equinox 55 spectrometer (Bruker, Germany). The spectra were collected in 400-4000 cm^{-1} wavenumber range with 4 cm^{-1} spectral resolution. The surface morphology and nanofibers' diameters were investigated by scanning electron microscopy (SEM). The employed equipment was VEGA 2 SEM

(Tescan, Czechia), and the micrographs were captured with 15.00 kV acceleration voltage.

Air filtration

The oil mist method was used to investigate the air filtration performance parameters of electrospun nanofiber membranes. This testing system consists of a pump, rotameter, ULPA filter, dust generator, filter holder, dust counter, and manometer (Figure 3). Each type of membrane individually was placed in a filter holder. At the

beginning of the test, internal airflow into the setup was purified by passing through a ULPA filter. Monodisperse dioctyl phthalate (DOP) particles with a diameter size of 300 nm were generated through an electrospray mechanism by a dust generator (ESP-3480 TSI) which was located before the filter holder. In this study, due to the importance of the size of exposed particles from the point of view of health and technology, the size of particles was considered 300 nm. This equipment generated aerosol with a concentration of 10^7 P/cm^3 and under the flow rate of 4 L/min. Dust counting was conducted before and after the filter holder by dust counter (Micro LPC), simultaneously flow rate and pressure drop were measured by a flow meter (model TA2) and rotameter (APM50K). All tests were carried out at

the air velocity of 5 cm/s. Finally, filtration efficiency (Equation 2), pressure drop (Equation 3), and quality factor (Equation 4) were calculated.

$$E = \frac{n_{in} - n_{out}}{n_{in}} \qquad (2)$$

In Equation 2, E refers to filtration efficiency, n_{in} is the quantity of aerosol particle before the filter holder, and n_{out} is the quantity of aerosol particle after the filter holder.

$$\Delta P = P_{in} - P_{out} \qquad (3)$$

In Equation 3, ΔP refers to the pressure drop, P_{in} is absolute pressure before the filter holder, and P_{out} is the absolute pressure after the filter holder.

$$Q = \frac{-\ln(1-E)}{\Delta P} \qquad (4)$$

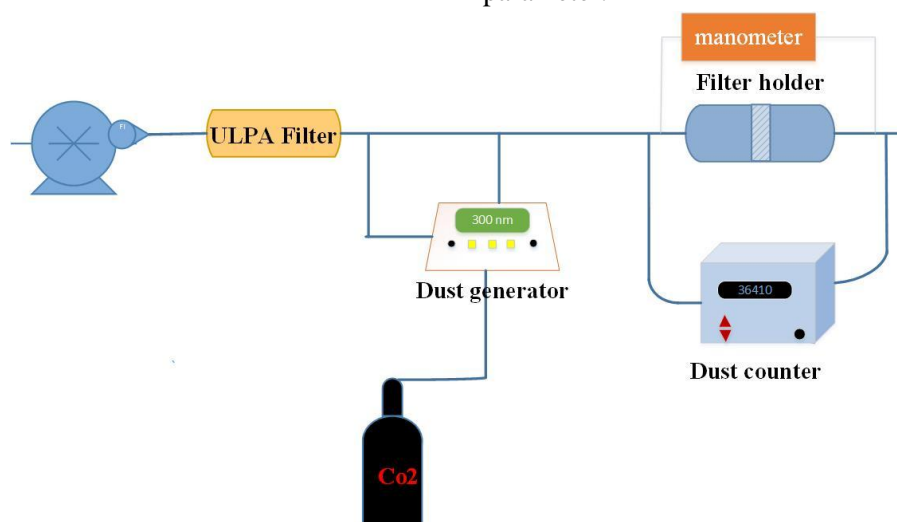In Equation 4, Q refers to quality factor parameter.

Figure 3: Measurement of filtration parameters in fabricated nanofibers

Toluene adsorption efficiency test

For the toluene adsorption experiment, pure and hybrid electrospun PU membranes with a surface area of 19.62 cm^2 were separately placed into a closed container with two valves based on ASHRAE standard, and surface velocity was set to 2 cm/s. According to Figure 4 (a), 50 ml toluene with 200 ppm concentration was transferred into the three-necked flask, which was located on the heater and allowed to evaporate. Before the reaching of vapor phase to the adsorption section, the concentration of toluene was balanced inside the

sealed uniform container. The required air was provided by a compressed air capsule, and the airstream was purified by separating interfering particles by HEPA filter and dehumidified through a high-performance dehumidifier (TSI- USA, model 3074). Finally, the concentrations of toluene were measured before and after the nanofiber media by Fho check (USA), and the toluene adsorption efficiency of nanofibers was determined. Figure 4 (b), indicates the actual membrane holder with inlet and outlet that the membrane has been located at the central part of the holder.
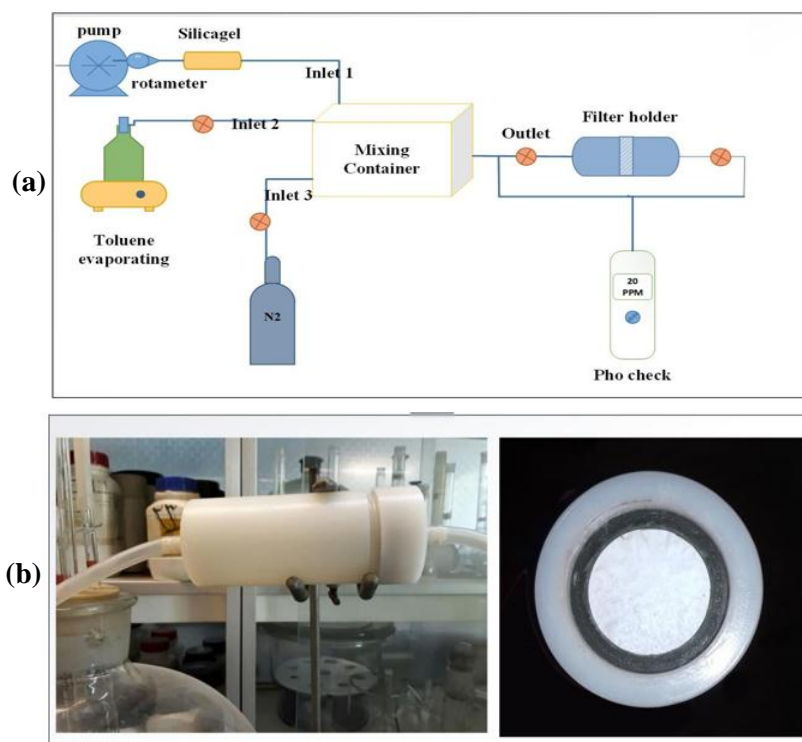
Figure 4: (a): Measurement of adsorption efficiency of fabricated nanofiber membranes,
(b): membrane holder (left), and cross-sectional view of the holder with electrospun membrane (right)

Statistical method

After collecting the data and entering to SPSS26, a regression test with the stepwise method was used to diagnose the relation between toluene adsorption and β-CD concentration.

Ethical issues

This research was completed in accordance with the ethical principles of, and was approved by, the research ethics committee of Tabriz University of Medical Sciences (IR.TBZMED.VCR.REC.1399.373).

Results

FTIR analysis

Figure 5 represents the results of FTIR spectroscopy. According to the spectra, spectroscopy of PTMG and the final PU mixture was carried out before and after curing. The elimination of isocyanate bonding characteristic (N=C=O) at a wavenumber of 2235 cm^{-1}, as well

as wavenumbers of 3227 and 3400 cm^{-1}, besides formation of –NH at a wavenumber of 3300 cm^{-1}, improved the reaction of PU.

Investigation of morphological characteristics of nanofiber membranes

Figure 6 reveals the SEM images of pure PU nanofiber and composite nanofibers, which were contained different amounts of β-CD. The diameter distribution is shown for each type of nanofiber. The electrospun pure PU nanofiber had a uniform and bead-free structure with an average diameter of 796 nm, while β-CD-containing nanofibrous membranes compared to pure PU membrane had smaller fiber diameters. The nanofiber membrane containing 3 wt% β-CD had the smallest diameter size (average diameter: 153 nm). According to the Figure 6, the morphology of PU/5 wt% β-CD was nonuniform and electrospun nanofiber diameter size increased at this concentration of β-CD.
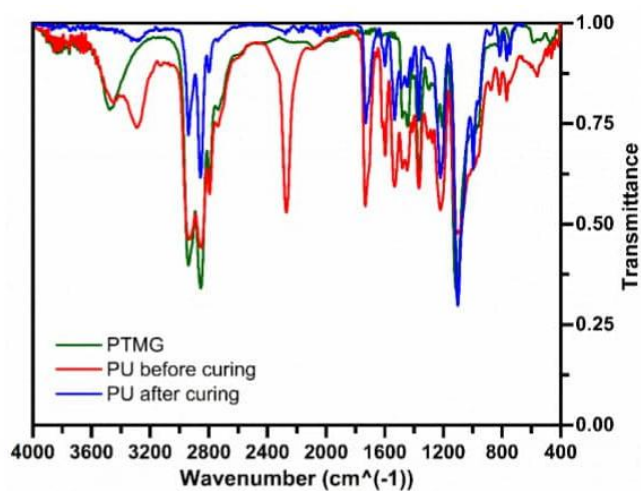
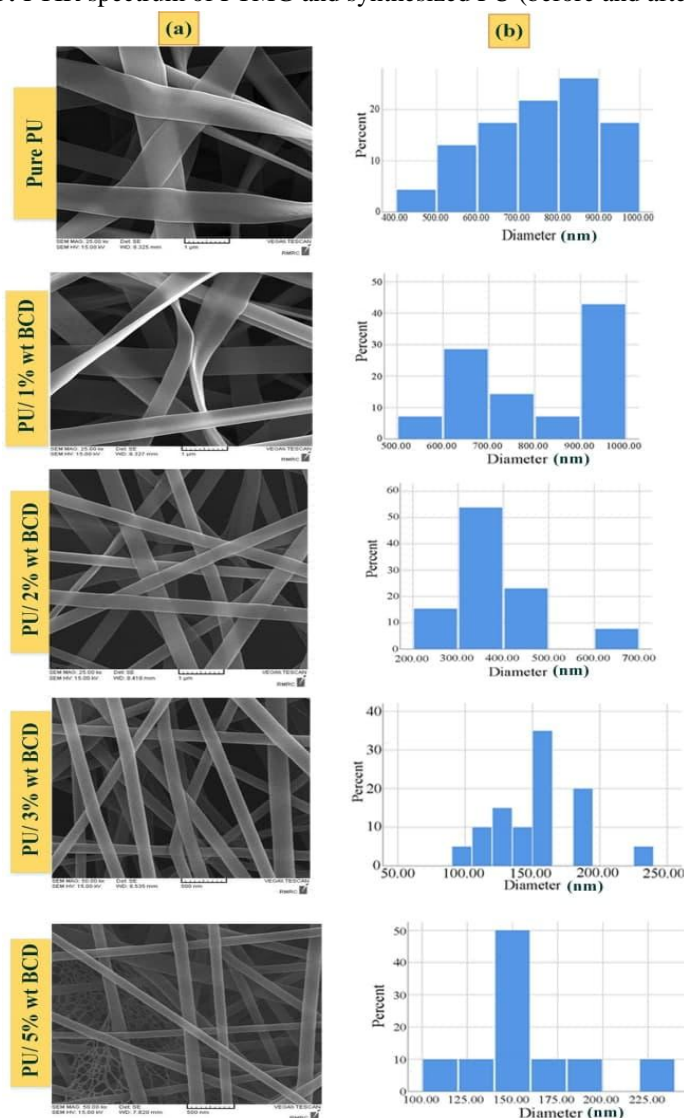**Figure 5:** FTIR spectrum of PTMG and synthesized PU (before and after curing)

Figure 6: SEM images, morphology (column a), and diameter size distribution (column b) of different electrospun nanofiber membranes

Air filtration

Figure 7 shows the filtration efficiency of various types of β-CD electrospun nanofiber membranes against DOP particles at a mean diameter size of 300 nm and 5 cm/s face velocity. According to the results of this figure, PU/3 wt% of β-CD nanofiber had the highest filtration efficiency (97.1%).
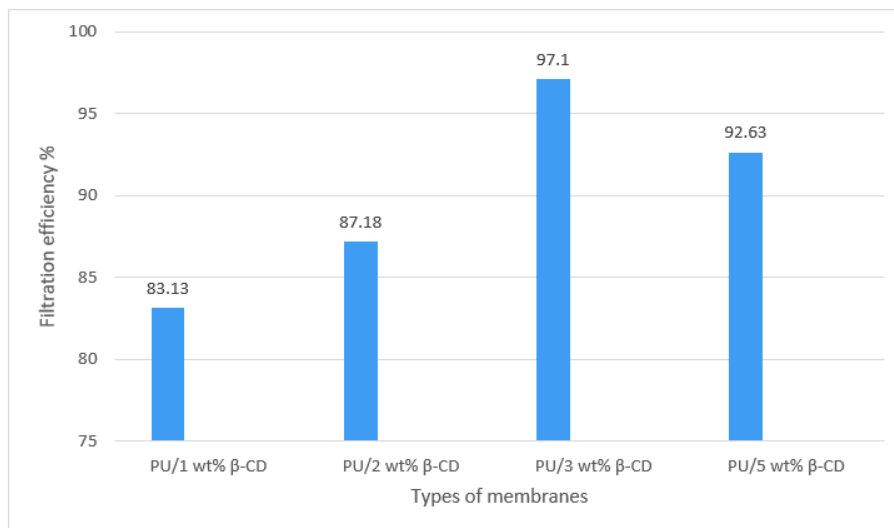

Figure 7: Percentage of filtration efficiency in composite nanofiber membranes

Figure 8 indicates the pressure drop parameter in different electrospun nanofibers for 0.3 µm particles at a face velocity of 5 cm.s^{-1}. PU/1 wt% of β-CD had the lower pressure drop. This parameter increased by increasing the amount of β-CD, , in which the PU/2 wt% of β-CD membrane had the highest pressure drop.
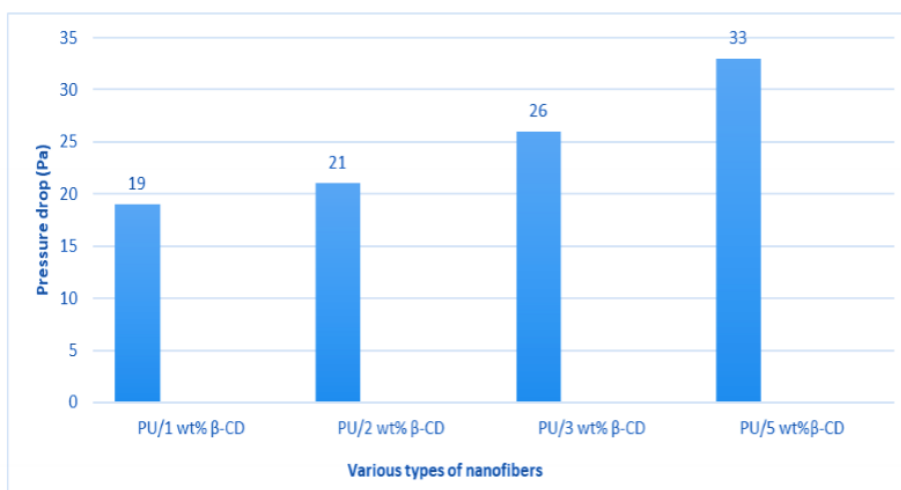

Figure 8: Pressure drop in composite nanofiber membranes

Figure 9 presents the quality factor of different types of nanofiber membranes for 0.3 µm particles at a face velocity of 5 cm.s^{-1}. Among different electrospun nanofiber membranes, PU/1 wt% of β-CD had the higest QF. This parameter decreased by increasing the amount of β-CD membranes, in which PU/2 wt% of β-CD had lowest QF.
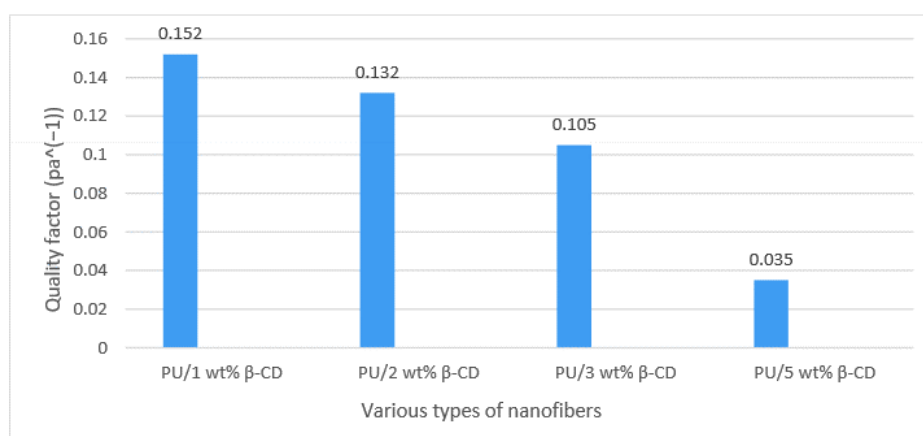
Figure 9: Quality factor in composite nanofiber membranes

Figure 10 demonstrates toluene adsorption capacity of different electrospun nanofiber membranes. Based on the results, the adsorption capacity of pure PU membrane increased by adding β-CD nanoparticles. This adsorption trend increased by adding the 3 wt% of β-CD into pure PU nanofiber, but increasing the concentration up to 5 wt% of β-CD had the reverse response. Figure 10 represents the adsorption capacity of AC, besides electrospun nanofibers. The capacity of PU/ 3 wt% β-CD and AC for toluene vapor was estimated at 72% and 84%, respectively.
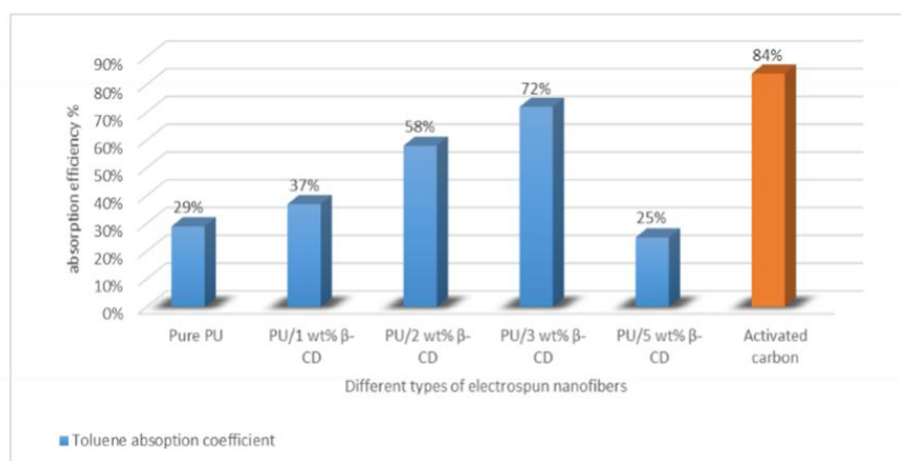

Figure 10: Toluene adsorption capacity of electrospun nanofibers and AC

In this study, a statistical regression model was drawn to determine the relationship between toluene adsorption and β-CD concentration and also to specify the optimal concentration of β-CD. The regression equation is the output of modeling as shown in Equation 5:

$$Adsorption = 22.7 + 31.2(\beta - CD) - 6.03(\beta - CD)^2 \qquad (5)$$

The coefficient of determination was 85.88% for the model. In other words, 85.88% of the variation in adsorption was defined by β-CD and $(\beta\text{-}CD)^2$ in the model. According to the model, the maximum adsorption (62.94%) was obtained at a β-CD concentration of 2.58%.

Discussion

FTIR spectroscopy was carried out to confirm the formation of PU by poly (tetramethylene ether) glycol (PTMG) as the soft segment, 1,4-butanediol (BDO) as the chain extender, and methylene diphenyl diisocyanate (MDI) as the hard

segment. Similar results have been reported in the literature analyzing synthesized PU spectroscopy [39,40].

The quantitative and qualitative results of nanofiber morphological analysis were recorded with SEM images. An important feature of electrospinning is that the morphology and diameter of nanofibers are changeable based on the electrospinning parameters [41]. The polymer concentration, flow rate, and voltage are the most critical factors that affect the morphology of nanofiber membranes [42]. By increasing the amount of β-CD in the electrospun solution, the mean diameter of β-CD nanofibers became smaller compared to pure PU nanofibers. It can be due to the grown conductivity and viscosity of PU/β-CD solution; a similar result has been reported by Kim et al [43]. Moreover, increasing the β-CD concentration up to the optimal level produced uniform and bead-free nanofibers. Therefore, increasing the β-CD concentration up to 3 wt% provided an effective nanofiber membrane. Increasing β-CD component into an electrospun solution up to 5 wt% caused the fabrication of non-uniform nanofibers with larger diameter. It was due to a significant difference in electrospinning solution viscosity.

Filtration is an important method for separating aerosols from the air by passing through the porous membrane [44]. In this approach, suspended particles, that are durable on the fiber of membrane by Vander valance links, are predominately captured by mechanisms, such as diffusion, inertial impaction, and direct impaction [45]. The performance of the filter is described by filtration parameters, which include collection efficiency and pressure drop. Figure 7 reveals the highest filtration efficiency (97.1%) in PU/3 wt% of β-CD nanofiber, which was correlated with the smallest fiber diameters. Nanofibers also showed lower efficiency (92.63%) compared to PU/3 wt% β-CD nanofiber (97.1%) for 0.3 μm particles, as observed in SEM micrographs (Figure 6). This reduction was attributed to the thicker fiber diameter of PU/5 wt% β-CD versus 3 wt% β-CD. By increasing the β-CD content, the pressure drop

increased noticeably in the samples from 19 Ps for 1 wt% β-CD to 33 Pa for 5 wt% at an air velocity of 5 cm/s. On the other hand, the pressure drop trend was almost similar for samples containing 1 wt% to 3 wt% β-CD. Slight fluctuations were observed in the pressure drop, increasing from 26 Pa for 3 wt% β-CD to 33 Pa for 5 wt% β-CD samples. The increase in pressure drop could be attributed to the increase in fiber diameter (Figure 6), pore size, and irregular structure as a consequence of the β-CD presence in the composite PU incorporated with 5 wt% β-CD nanofiber.

Quality factor (QF) can be used as an indicator to measure the filtration performance of fibrous filters, also known as the figure of merit, which is the ratio of the penetration rate of particles to pressure drop across the filter [46]. QF is a function of filtration efficiency and pressure drop, which reflects the cost-benefit principle, where the cost refers to pressure drop (a cause of significant energy consumption) [47] and benefit refers to filtration efficiency. As a practical role, an excellent filter should provide maximum filtration efficiency and minimum pressure drop. Nanofibers with significant QF show high quality and performance. 1 wt% β-CD nanofiber membranes, due to their lower pressure drop and desirable filtration efficiency, had a significant QF. Generally, air filters with higher filtration efficiencies because of the smaller pore size are more easily blocked [48]. Although the PU incorporated with 5 wt% β-CD membrane had a rather higher filtration efficiency, the increased pressure drop was the cause of lower QF owing to less porosity.

The mechanism of filter purification against particles and gas contaminants is completely different. In other words, a particle is captured upon interception with a nonwoven fiber owing to its large aerodynamic diameter and high inertia. Meanwhile, a gaseous contaminant can pass through the porosity of non-treated nonwoven fiber due to its smaller size and lower inertia. Therefore, to enhance the performance of nanofiber membranes, these nanomembranes should be

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embedded with substances, such as nanoparticles that can adsorb unfavorable gases and vapors. The adsorption performance of a PU nanofiber is strongly related to parameters, such as the morphology of pore and diameter of polymer, which change depending on the content of additives. Importantly, when the diameters of polymer fiber materials decrease from micrometers to sub-microns or nanometers, several surprising characteristics arise. They include a very large surface-area-to-volume ratio, flexibility in surface functionality, and superior mechanical performance to other known materials. Therefore, improved adsorption/ desorption performance is expected from electrospun nanofibers due to their small diameter and high porosity.

Toluene is an aromatic hydrocarbon, composed of a benzene ring linked to one methyl group. It has been used as a solvent or a chemical intermediate in various industrial applications. As shown in Figure 10, an increase in the β-CD content leads to an increase in the adsorption capacity of composites. Except for the sample containing 5wt% β-CD, the adsorption efficiency of all composite nanofibers was higher than the pure PU nanofiber membrane. The highest adsorption efficiency was obtained when 3 wt % β-CD was combined with PU nanofiber. As can be seen in Figure 10, samples containing more β-CD showed a higher adsorption capacity in the composites. Therefore, the adsorption capacity depends on several important parameters, including β-CD content, pore morphology, and diameter of polymer. Overall, these parameters determine the final adsorption capacity of the composite.

According to Figure 10, PU/3 wt% β-CD shows the highest adsorption efficiency among all membranes tested. By adding 3 wt% β-CD, toluene adsorption further improved by 72%, which can be attributed to the cavities of β-CD trapping toluene. However, the addition of 5 wt% β-CD did not improve toluene adsorption. Adsorption is dramatically improved when β-CD is added to nanofibers, leading to a decrease in

the fiber diameter and an increase in the specific surface area. If the adsorption efficiency is determined per surface, it changes by adding β-CD, which may be due to variations in pore morphology and polymer diameter. Samples with weight percentages of 3 wt% and 5 wt% exhibited the maximum and minimum adsorption efficiencies, respectively. Therefore, optimal adsorption efficiency was obtained at a weight percentage of 3 wt%, indicating the efficacy of β-CD as a candidate for adsorption of pollutants. Decreased adsorption efficiency after adding 3 wt% to 5 wt% can be attributed to higher polymer matrix viscosity, causing stiffness and mass formation. A previous study demonstrated that the membrane cross-linked with β-CD powder could adsorb hazardous and carcinogenic VOCs, such as xylene, benzene, and formaldehyde [49]. Also, Kadam et al. reported that the adsorption of HCOH through β-CD powder was higher than PAN powder. Significant adsorption was reported in the electrospun PAN/ β-CD membrane due to thin fiber diameter, large surface area, and high affinity of β-CD to form a complex [50].

It can be concluded that β-CD absorbs toluene via two mechanisms. The cone-shaped β-CD contains a hydrophobic cavity with a specific diameter and depth [51]. In the first approach, according to the structure of β-CD, the formation of the π complex occurs in the β-CD cavity (host) to capture toluene as a guest molecule. In the other adsorption mechanism, toluene is captured by bonding OH groups, which surround the exterior structure of β-CD cavity. Overall, increasing the concentration of β-CD up to an optimal level in the nanofiber membrane enhances toluene adsorption. This nanoparticle shows different tendencies to capture a variety of VOCs.

The capacity of PU/ 3 wt% β-CD and AC for toluene vapor was estimated at 72% and 84%, respectively. Moreover, it was observed that PU/ 3 wt% β-CD nanofiber membranes (0.22 g) had acceptable efficiency for capturing toluene vapor in comparison with the AC absorbent (0.46 g). Therefore, the synthesized multilayer nanofiber

can be an appropriate substitute for the AC adsorbents because of lower pressure drop, large surface, and lower weight.

Conclusion

Herein, PU/ β-CD nanofiber membranes were fabricated via the electrospinning process for air filtration and toluene adsorption. Adding β-CD to the PU solution produced nanofibers with different morphological characteristics. The thinner diameter and the thicker diameter contained 3 Wt% and 5 Wt% of β-CD, respectively. Among five electrospun membranes, the highest QF was obtained for PU/1 wt % β-CD membrane. This membrane could capture particles with a 300 nm diameter owing to its lower pressure drop (19 Pa) and acceptable filtration efficiency (83.13%), which was important in terms of health and technology.

The results of this study also showed that the nanofiber membrane containing 3 wt% β-CD had the highest adsorption efficiency of toluene. In this type of membrane, β-CD adsorbs toluene by forming a host-gest complex. According to the statistical regression model, the maximum toluene adsorption (62.94%) was obtained when the β-CD concentration was 2.58%.

Moreover, it was found that PU/3 wt% β-CD nanofiber membrane had acceptable efficiency to capture toluene vapors compared to the AC absorbent. Therefore, multilayer synthesized composite nanofibers, due to less pressure drop and efficient adsorption capacity could be an appropriate option substitute for AC.

According to the findings, synthesized PU/ β-CD nanofiber media, due to significant efficiency to capture toxic evaporations of VOCs and particle filtration, can be an appropriate and practical option for people who are exposed to indoor or outdoor aerosol and gaseous contaminants, such as hospital personnel, traffic police, and patients with respiratory disorders.

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Conflicts of interest

The authors declare that there is no conflict of interest.

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